

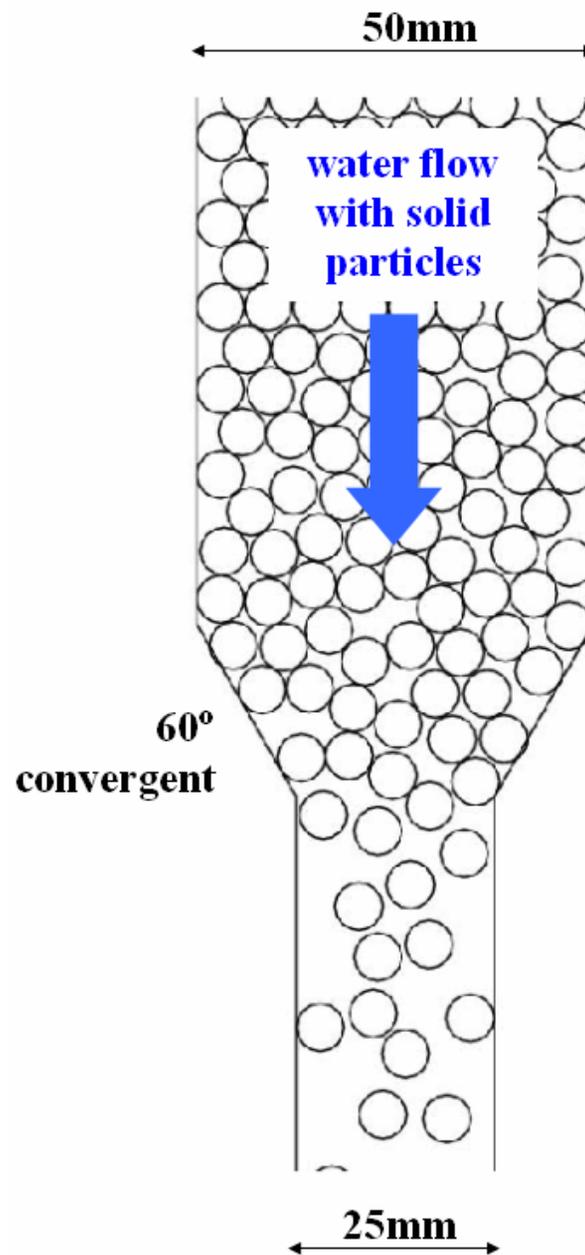
# Modeling of accumulation of particles upstream of conduit constrictions

- high concentration, large and cohesionless particles

Andrew Parry

**Schlumberger**

# Granular and liquid flow



- $\rho_p/\rho_f \sim 2$
- $0 < d_p < \sim 5\text{mm}$
- $0 < U_f < \sim 1\text{m/s}$
- **high solids loading**

# Outline

- **Model without flow forces**
- Model with algebraic flow forces and prescribed fluid velocity distribution
- Model with algebraic flow forces and fluid velocity distribution from numerical solution to flow field
- Conclusions and perspectives

Multi-body dynamics algorithm of Fortin, Millet and de Saxcé\*

- implicit with non-smooth contact dynamics

for this presentation a 2D mono-dispersed version without cohesion forces is used

$$\vec{U}_p^{n+1} = \vec{U}_p^n + \frac{1}{m} \left( \vec{F} \delta t + \sum_c \vec{S}^{n+1} \right)$$

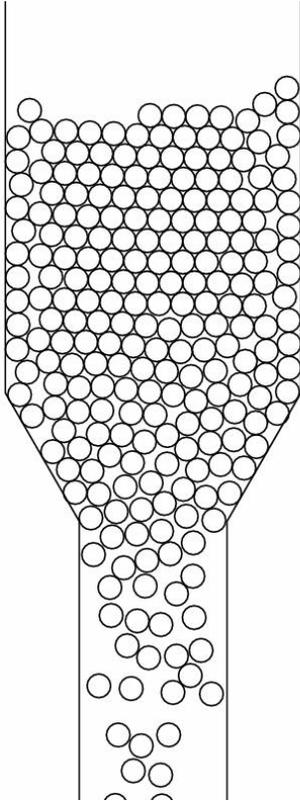
$$\omega_p^{n+1} = \omega_p^n + \frac{1}{I} \sum_c S_\omega$$

where  $\vec{S}$  and  $S_\omega$  are the translational and rotation impulses due to collision  $c$

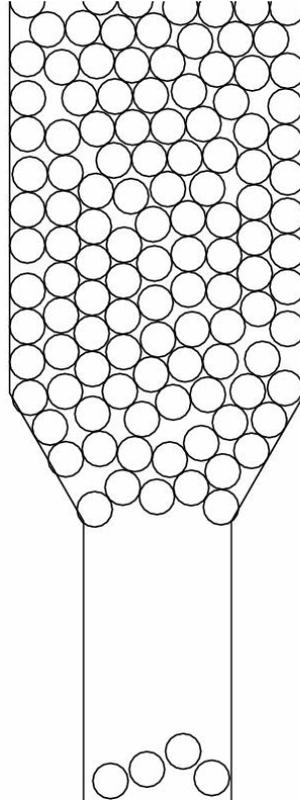
\*J. Fortin, O. Millet and G. de Saxcé, 'Numerical prediction of granular materials by an improved discrete element method', Int. Jou. for Num. Meth. in Engineering, 2005, 62:639-663

# Result animations for gravitation flows without fluid forces

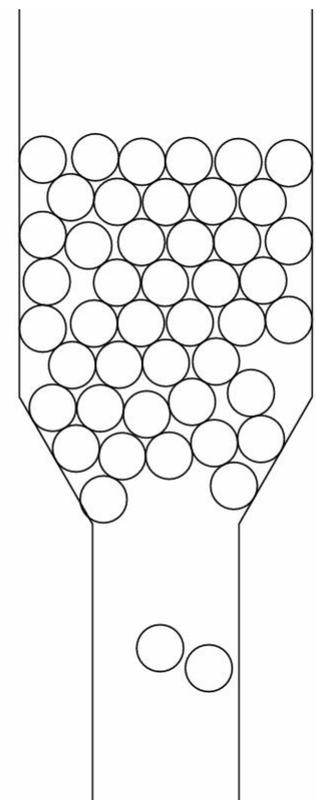
$d_p = 4\text{mm}$



$d_p = 6\text{mm}$



$d_p = 8\text{mm}$



$\rho_p = 1000\text{kg/m}^3$ , normal and tangential restitution coefficients = 0.8, 0.9

friction coefficient = 0.5

# Outline

- Model without flow forces
- **Model with algebraic flow forces and prescribed fluid velocity distribution**
- Model with algebraic flow forces and fluid velocity distribution from numerical solution to flow field
- Conclusions and perspectives

Flow forces from semi-empirical relation by Ergun\*

$$\vec{F} = \frac{\pi\mu d_p}{6\varepsilon^3} (150(1 - \varepsilon) + 1.75R_{ep}) (\vec{U}_f - \vec{U}_p)$$

where  $\mu$  is the fluid viscosity and  $\varepsilon$  is the void fraction

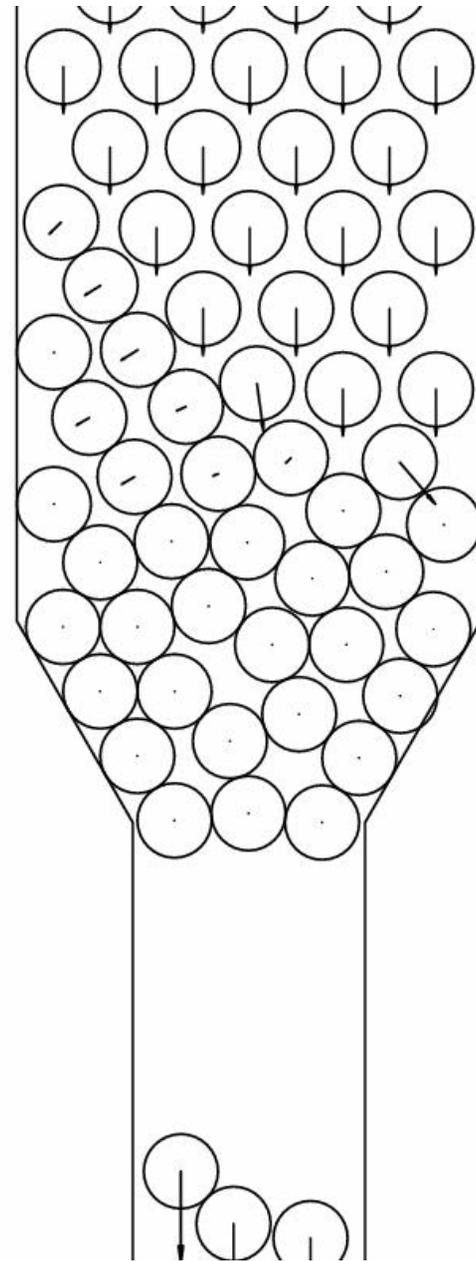
\*S. Ergun, 'Fluid flow through packed columns', Chem. Eng. Prog.,  
48(2):89-94, 1952

Result animation for:-

1m/s water superficial

velocity

$d_p = 8\text{mm}$

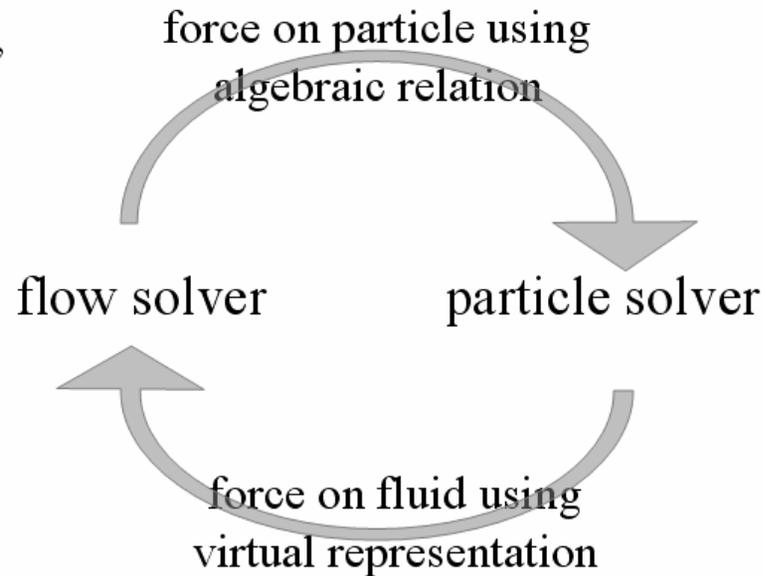


# Outline

- Model without flow forces
- Model with algebraic flow forces and prescribed fluid velocity distribution
- **Model with algebraic flow forces and fluid velocity distribution from numerical solution to flow field**
- Conclusions and perspectives

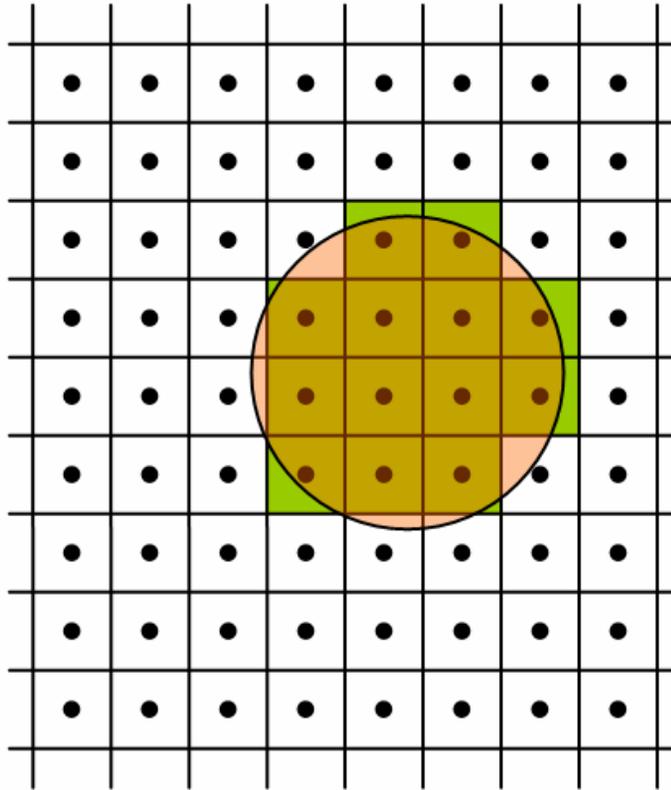
# Application of the PSI-Cell method of Crowe et al.\* to large particles

during each time step;



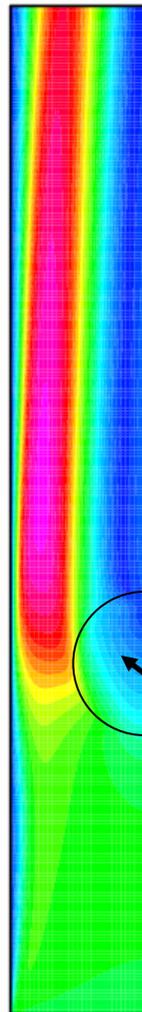
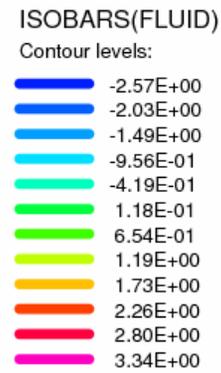
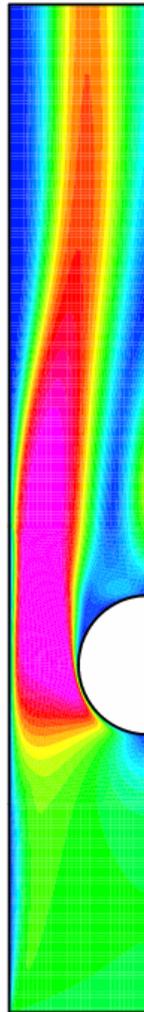
\* C. T. Crowe, M. P. Sharma and D. E. Stock, 'The Particle-Source-In-Cell (PSI-Cell) Model for Gas-Droplet Flow, J. Fluids Engin., 1977, 325-332

# Virtual representation of solid within the fluid

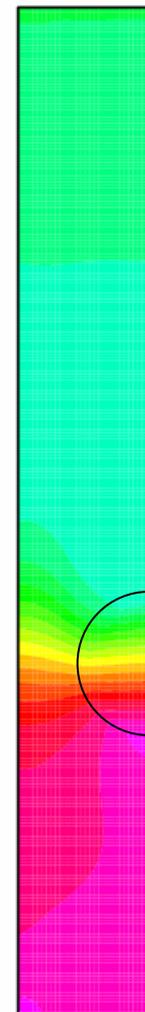
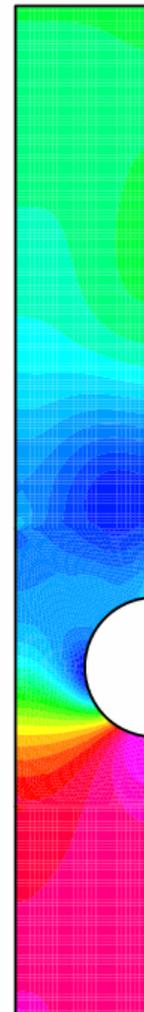


1. Stair-case representation of cylinder  
orange cylinder -> set of green cells
2. Force on fluid acting from cylinder  
is distributed over all green cells

# Test of flow past a confined cylinder, $Re_p = 400$



fluid momentum  
source from real  
representation



# Outline

- Model without flow forces
- Model with algebraic flow forces and prescribed fluid velocity distribution
- Model with algebraic flow forces and fluid velocity distribution from numerical solution to flow field
- **Conclusions and perspectives**

2D predictions of mono-dispersed particles transported through a conduit reduction without cohesion show

- Blockage of conduit by bridging/arching upstream of reduction, without and with fluid forces acting on the particles
- A critical particle size above which bridging occurs

Work on methodology for particle interaction with numerically generated flow field based on extension of PSI-Cell method is in progress

# Acknowledgements

I wish to thank Professor A. Hamdouni and Professor O. Millet of LEPTAB, Université de la Rochelle for their advice and fruitful discussions